directing elements, the directing elements of the second row being arranged at said angle (γ) relative to the directing elements of the first row.

7. (Amended) A fluid conveying tube as claimed in claim 1, wherein said angle (γ) is about 20-100°.

9. (Amended) A fluid conveying tube as claimed in claim 1, which is designed to be passed by a liquid, wherein the centre-to-centre distance between directing elements succeeding in said longitudinal direction is about 10-40 times as large as the height of the directing elements perpendicularly to the primary surfaces.

10. (Amended) A fluid conveying tube as claimed in claim 1, which is designed to be passed by a gas, wherein the centre-to-centre distance between directing elements succeeding in said longitudinal direction is about 25-65 times as large as the height of the directing elements perpendicularly to the primary surfaces.

Please also add the following new claims 15-20:

--15. A fluid conveying tube as claimed in claim 1, wherein said angle (γ) is about 30-90°.--

--16. A fluid conveying tube as claimed in claim 1, wherein said angle (γ) is about 90°.--

--17. A fluid conveying tube as claimed in claim 1, which is designed to be passed by a liquid, wherein the centre-to-centre distance between directing elements succeeding in said longitudinal direction is about 15-35 times as large as the height of the directing elements perpendicularly to the primary surfaces.--

--18. A fluid conveying tube as claimed in claim 1, which is designed to be passed by a gas, wherein the centre-to-centre distance between directing elements succeeding in

said longitudinal direction is about 30-55 times as large as the height of the directing elements perpendicularly to the primary surfaces.--

--19. A fluid conveying tube as claimed in claim 1, wherein said elongate directing elements are arranged obliquely with respect to the longitudinal direction of the primary surfaces.--

--20. A method of effecting heat transfer in a heat exchanger, comprising:

introducing a plurality of partial flows into a heat exchanger tube, the tube defining a longitudinal axis and

imparting to each of said partial flows a swirling motion about the longitudinal axis.--